

# Blyth Sewage Treatment Plant Annual Report 2015

The following is a summary and discussion of the 2015 operating year of the Blyth Sewage Treatment plant and a summary of compliance limits as set forth in the Certificate of Approval.

There are many concepts used to monitor the process and efficacy of sewage treatment plants that are analysis driven. The simplistic approach used at the Blyth plant is based on dissolved oxygen, final effluent total ammonia and dissolved phosphorous concentrations to determine process conditions. Since the nitrifying biology is sensitive, they are used as an indicator and an upset of the plant can be quickly identified through an increase in ammonia levels and either a sharp drop or increase in the respiration rate as indicated by the dissolved oxygen. Dissolved phosphorous concentrations are monitored to determine appropriate ferric chloride dosages and periodic mixed liquor suspended solids are performed to adjust available biomass for treatment.

# The Rated Capacity of the Treatment unit at 730m3/day

Based on Raw sewage flows, the 2015 annual average flows were 393.7m3/day which represents 54% of the annual average 730m3/day capacity. This represents a 9.5% decline compared to last year

### By- pass Events

There were five by-pass events in 2015 at the Blyth sewage treatment plant where secondary by-passes needed to take place, all five by-pass events were measured events. The longest by-pass event was in November for a total of 56 hours which was for the replacement of an aeration pipe and cleanout. The total number of bypass hours for the year was 101.25 hours with a cumulative volume of 4351m3

### **Compliance limits**

The plant operated within Regulatory Compliance limits throughout the year.

### **Operational problems**

Aeration basin #1 required a diffuser header to be repaired in which it was removed from service creating a secondary bypass event due to bypassing a small portion of the treatment which was reported to MOECC. The pipe was repaired and has been working efficiently since with the root cause of the break found to be an unexpected accumulation of rags on the headers. The maintenance frequency of cleaning the basins is going to be increased to no more than a 2 year period to minimize the risk of reoccurrence.

#### Maintenance

Routine maintenance was performed such as oil changes in the gear drives, emergency generator and inspection of the pumps. Aeration basin 1 was cleaned and inspected. A new pH probe was purchased and installed for final effluent monitoring. Return pump 2 had failed and found to be a wiring issue where it was repaired, tested and placed back in service. An extension was added to the flowmeter level transmitter to minimize erroneous readings.

### Quality control monitoring

Monitoring includes an online dissolved oxygen sensor which indicates loading, raw sewage quality, aeration basin content and proper operations of the aerators. Secondary clarifier effluent is monitored for dissolved phosphorous and ammonia to determine adequate ferric chloride dosage and nitrification in the aeration basins as well as general clarity and surface debris which indicated proper solids removal, adequate solids return to the aeration and wasting rates.

Results of monitoring activities can be viewed on the monthly spreadsheets.

### Calibration and Maintenance

Calibration of the flowmeter was completed by ICS Instrumentation (after transducer extension was installed. pH analyzer calibration is checked on a monthly basis.

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# Certificate of Approval #8687-826L6Z issued February 9, 2010

**Efforts to Meet Effluent Objectives** 

As described in the Quality Control Monitoring section, analytic and visual parameters are used as indicators of process efficiency and should fall within the Critical Control Points. A summary of these values was developed and is in the Blyth Sewage Treatment Facility Operations Manual for reference and historically have been adequate to maintain compliance.

With the exception of a partial treatment bypass to repair air header in basin 1, there were a number of tertiary bypasses as a result of extraordinary precipitation and suspected sump pump connections. During high flows that exceed the solids removal capacity of the clarifier, the air is shut off in the second aeration section to greatly reduce the solids loading on the clarifier and to retain the solids.

The filter has been assessed and is in much better shape than the filter that had structural failure. The conclusion of the inspection was that there was no imminent danger of failure but that plans should be put in place for its replacement.

### **Biosolids Generated**

There was 696.2 m³ of biosolids removed from the storage tank in 2015 and utilized in accordance with NASM approval 5060206 for Farm 1 issued by Ministry of Agriculture, Food and Rural Affairs as developed by Crop Quest (NASMPDC1104) and applied by S&S Trucking.

### **Complaints**

There were no complaints received as a result of the operation of the sewage treatment facility

Included in this report is a Blyth sewage data summary, compliance summary, biosolids removal summary and bypass events summary

This report was prepared by:

K.McD

Kyllie McDonagh,

Compliance coordinator, QMS Rep, Administrative Assistance

Flow s	January	February	March	April	May	June	July	August	September	October	November	December	Total	Ava Flow	Mission	,0 ,0
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By-passing				748		2992					611		4354 mg	Ç		
Type			S	sec	S	sec					sec		2	2		
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													ΙĄ	Average	Max.	Removal
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SS	127	104	26	167	124	147	159	133	217	25.5	111	130		133.13	308	98.6
<u>L</u>	3.30	3.44	2.46	3.58	2.95	2.02	3.96	3.80	7.97	4.97	2.87	3.14		370	707	90.0
NA NA	31.35	37.85	22.43	35.10	44.90	26.45	26.05	29.30	48.05	38.30	29.30	27.45		33.04	18.78 AB.05	0.08
됩	7.75	8.17	8.03	7.62	7.91	7.86	7.67	7.54	7.29	7.97	8.02	7.92		7.81	8.17	90.1
Final Effluen	January	February	March	April	May	June	Auly	August	September	October	November	Danambar	174	A cocoo	Max	
CBOD	2.0	2.0	2.0	2.0	2.0	2.0	2.0	3.0	2.0			200	2	- 5	7Y.	
SS	2.0	2.0	4.7	2.5	2.0	2.0	2.0	2.0	2.0	2.0	2.0	20		2 20	787	
Ammonia	0.10	0.10	0.10	0.10	0.10	0.15	0.10	0.10	0.10	0.10	0.10	0.10	$\frac{1}{1}$	0 40	4.0	
NY.	0.95	1.10	0.67	1.10	0.50	0.85	1.20	2.65	0.75	1.37	0.85	5.15		143	7. C. T.	
٩	0.18	0.15	0.25	0.21	0.23	0.17	0.22	0.17	0.15	90.0	0.09	0.38		010	0.38	
NOZ	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03		003	0 0	
NO3	21.35	28.30	15.63	20.35	19.00	15.70	34.85	32.90	30.80	24.33	26.00	28.35		24.80	34.85	
F.	7.21	7.77	7.72	7.27	7.27	7.31	7.14	7.19	7.33	7.85	7.67	7.42	H	7 43	7 85	
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Actual	490	48	1279	1363	51	4 167	1 43	33 37	0 36	9 472		6:
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Actual	366			568	36:	3 51						73
Comp. Y/N	Y		Y	Y	)	′ `		Y		Y Y	412 Y	39
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CBOD	2.0									5 5		1
TSS	2.0	2.									2.0	2.
Loading Kg	11	1		11	3.7						2.0	2.
CBOD Kg	0.73	0.98			0.73				-		3.7	1
TSS Kg	0.73	0.98			0.73		-				0.82	0.7
Comp. Y/N	Y	γ		1.42 Y	0.73 Y						0.82	0.7
			·		T	Y		( Y	1	′ Y	Y	`
Tot P	1		1 1	1	0.3	0.3	0.3	2 00				
Actual	0.18	0.15	0.25	0.21	0.23						1	
TP Load Kg	0.7	0.7	0.7	0.7	0.2	0.17					0.09	0.40
Act. TP Kg	0.07	0.07	0.12	0.12	0.08		- 17				0,2	0.1
Comp. Y/N	Y	Υ	Υ	Y	Y	y y					0.04	0.18
·								<u> </u>		1 1	Y	<u> </u>
VH 3&4	17	21	14	6	3	1	-	1	1	3		
Actual	0.10	0.15	0.13	0.12	0.12	0.12	0.14			-	3	11
Comp. Y/N	Y	Υ	Y	Y	Υ	Y	Y		0.11 Y		0.11 Y	0.23 Y
VH 3	0.02	0.02	0.00								<u> </u>	<u> </u>
Actual	0.0002	0.002		0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02
Comp. Y/N	0.0002 Y	0.0002 Y	0.0003 Y	0.0003	0.0006	0.0010	0.0004	0.0008	0.0007	0.0069	0.0009	0.0006
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ot CI Res	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.0			
Nonth Max.	0.19	0.18	0.18	0.19	0.18	0.18	0.15		0.2	0.2	0.2	0.2
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	<u> </u>	ı	Y	Y	Y	Y	Y	Y	Y	Υ	Y	Υ
. Coli	200	200	200	200	200	200	200	200	200	000		
ctual GMD	2	14	0	8	3	3	10	6		200	200	200
omp. Y/N	Y	Υ	Y	Y	Y	Y	Y	Y	183 Y	18 Y	9 Y	18

Quarterly	ivietais Cal	culations R	eport		2015			
Paramete	r							
Date		Mar 31-15	May 27-15	July 8-15	Jul 28-15	Nov 9 15	Avorogo	
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NH 3&4		101	272	507	540	3.6	284.72	I
TKN		2110	1610	1940	1980	422	1612.4	
NO2		0.8	4.7	0.2	0.2	0.8	1.34	
NO3	<	0.3	0.3	0.3	0.2	1.1	0.46	
NO2+NO3		0.8	4.7	0.3	0.3	1.1	1.6	
Arsenic	<	0.3	0.3	0.2	0.3	0.1	0.24	
Cadmium	<	0.058	0.01	0.013	0.035	0.005	0.0242	
Cobalt		0.41	0.26	0.25	0.34	0.003	0.0242	
Chromium	1	3.8	2.4	2.6	3.5	0.78	2.616	
Copper		13	8.8	9.7	14	2.5	9.6	
Mercury		0.022	0.016	0.02	0.022	0.002	0.0164	
Potassium		170	130	130	150	75	131	
Molybden	<	0.31	0.23	0.24	0.1	0.08	0.192	
Sodium						0.00	#DIV/0!	
Nickel		1.2	0.76	0.84	1	0.25	0.81	
Phosphoro	ous	1300	920	950	1200	220	918	
_ead		1	0.5	0.6	0.5	0.2	0.56	
Selenium	<	0.1	0.1	0.1	0.3	0.1	0.14	
Zinc		21	13	13	18	3.4	13.68	
Ecoli DW		19182	10511	5538	6005	941748	196596.8	-
Ecoli /100	ml	75000	35000	18000	23000	970000	224200	
ank in " t	о Тор							
olume in	m3	941	941	941	941	941		
olume at	4%	920	784	765	901	242	0	
olids Kg		36801	31342	30589	36048	9694	0	

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STP         SB         940         5.5         0.372         M         Y         Y         T           STP         SB         23.00         16         0.749         M         Y         Y         1           STP         SB         330         23.75         1.871         M         Y         Y         4           STP         SB         5:00         56         0.611         M         Y         Y         4           STP         SB         5:00         56         0.611         M         Y         Y         4           STP         SB         5:00         56         0.611         M         Y         Y         Y         4           STP         SB         5:00         56         0.611         M         Y <td></td> <td></td> <td></td>			
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y Bypass         M = Measured         *Reason           day Bypass         M = Measured         Y = Yes         1 = Heavy Precipitation           wage Treatment Plant Overflow         3 = Infiltration         3 = Infiltration         4 = Mechanical/ Equipment Failure           tary Sewer Overflow         5 = Pipe Failures(break/ leak/ plugged)         5 = Pipe Failures(break/ leak/ plugged)			
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wage Treatment Plant Overflow       3 = Infiltration         bined Sewer Overflow       4 = Mechanical/ Equipment Failure         tary Sewer Overflow       5 = Pipe Failures(break/ leak/ plugged)         tellite Treatment Works Overflow	7 = Power Outages		
bined Sewer Overflow 4 = Mechanical/ Equipment Failure tary Sewer Overflow 5 = Pipe Failures(break/ plaged) tellite Treatment Works Overflow	8 = Unknown		
karj sewer Overnow 5 = Pipe Failures(break/ leak/ plugged) Itellite Treatment Works Overflow	9 = Other, please comment below.		
Comments:			

	Primary Bypass			Secondary	Bypass		Plant Over	flowe		0 " "		
MONTH	No. of Events (events)	Duration (hours)	Volume (1000m3)	No. of Events (events)	Duration (hours)	Volume (1000m3)	No. of Events (events)	Duration (hours)	Volume (1000m3)	No. of Events (events)	Duration (hours)	Volume (1000m3
January	0			0			0					
February	0			0			0			0		
March	0			0						0		
April	0			1	11.6	0.748	0			0		
May	0			0	11.0	0.740	0			0		
June	0			3	30.2	2.992	0			0		
July	0			0	30.2	2.992	0			0		
August	0			0			0			0		
September	0			0			0			0		
October	0			0			0			0		
Vovember	0			1	56		0			0		
December	0			0	36	0.611	0			0		
							0			0		
OTAL	0	0	0	5	97.8	4.351	0	0	0	0	0	
Γο be submit	ted quarterly, v	ithin 45 days	of the end of	the quarter.								and the second second second second
	ent' means an				or overflow se previous ev	parated by a prent, at each l	period of more ocation.	than 12 hou	s between the	e occurrence(s	s) or the ever	nt(s) and th